

Magnetic MoS₂/Fe₃O₄ composite as an effective activator of persulfate for the degradation of tetracycline: performance, activation mechanisms and degradation pathways

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ABSTRACT

The activated persulfate (PS) process could produce sulfate radical (SO₄^{•-}) and rapidly degrade organic pollutants. The application of Fe₃O₄ as a promising PS activator was limited due to the rapid conversion of Fe²⁺ to Fe³⁺ on its surface. Mo⁴⁺ on MoS₂ surface could be used as a reducing site to convert Fe³⁺ to Fe²⁺, but the separation and recovery of MoS₂ was complex. In this study, MoS₂/Fe₃O₄ was prepared to accelerate the Fe³⁺/Fe²⁺ cycle on Fe₃O₄ surface and achieved efficient separation of MoS₂. The results showed that MoS₂/Fe₃O₄ was more effective for PS activation compared to Fe₃O₄ or MoS₂, with a removal efficiency of 91.8% for 20 mg·L⁻¹ tetracycline (TC) solution under the optimal conditions. Fe²⁺ and Mo⁴⁺ on MoS₂/Fe₃O₄ surface acted as active sites for PS activation with the generation of SO₄^{•-}, •OH, •O₂⁻, and ¹O₂. Mo⁴⁺ acted as an electron donor to promote the Fe³⁺/Fe²⁺ cycling and thus improved the PS activation capability of MoS₂/Fe₃O₄. The degradation pathways of TC were inferred as hydroxylation, ketylation of dimethylamino group and C-N bond breaking. This study provided a promising activated persulfate-based advanced oxidation process for the efficient degradation of TC by employing MoS₂/Fe₃O₄ as an effective activator.

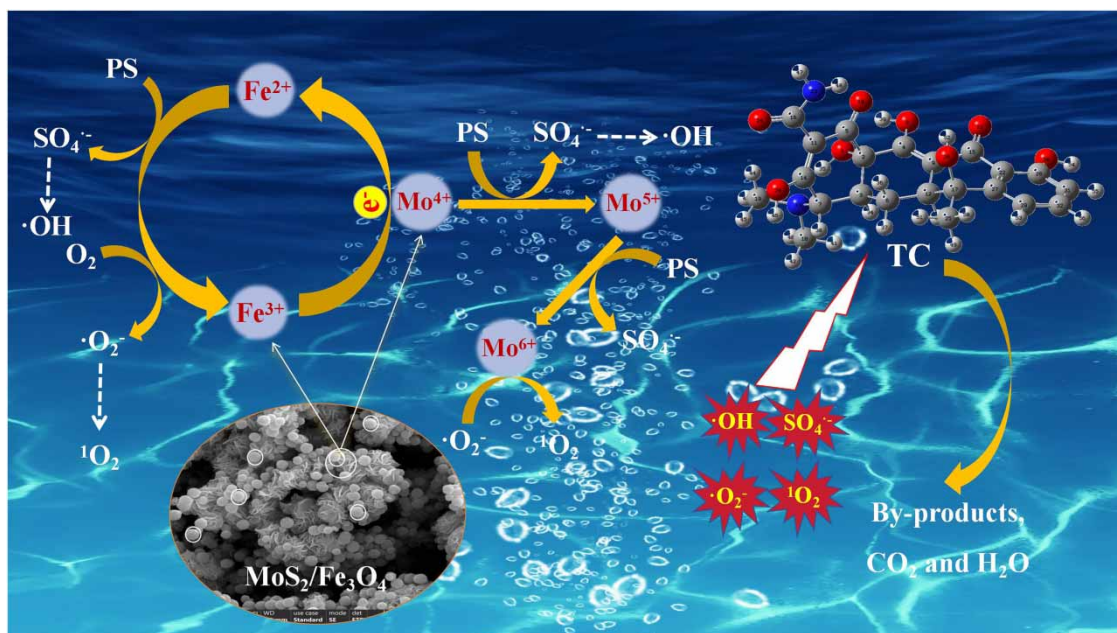
Key words: activation, Fe₃O₄, MoS₂, persulfate, tetracycline

HIGHLIGHTS

- MoS₂/Fe₃O₄ was an effective, recoverable PS activator for tetracycline degradation.
- TC was removed by free radical and non-free radical degradation pathways.
- Mo⁴⁺ promoted the regeneration of Fe²⁺ on the Fe₃O₄ surface.

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GRAPHICAL ABSTRACT



1. INTRODUCTION

Tetracycline (TC), as a broad-spectrum drug, has been widely prescribed for the treatment of bacterial infections in humans and animals (Peng *et al.* 2022). However, only a small portion of TC is absorbed and digested by organisms, while the residue is discharged into the water ecosystem, leading to the occurrence of drug-resistant bacteria and posing a great threat to human health (Cheng & Ji 2022; Liu *et al.* 2022b). Consequently, it is necessary to remove TC from the wastewater (Neolaka *et al.* 2023; Zhang *et al.* 2023d).

Persulfate (PS)-based advanced oxidation processes (AOPs) are considered as an effective method for decomposing pollutants due to their ability to produce sulfate radical ($\text{SO}_4^{\bullet-}$) (Wang *et al.* 2023). Compared with hydroxyl ($\cdot\text{OH}$), $\text{SO}_4^{\bullet-}$ produced by the activated PS has a higher redox potential (2.5–3.1 V) (Zhou *et al.* 2023) and a longer lifetime (30–40 μs) (Wang *et al.* 2022; Shabanloo *et al.* 2023), which is conducive to the degradation and mineralization of the pollutants due to sufficient time provided for $\text{SO}_4^{\bullet-}$ diffusion and contact with organic pollutants. $\text{SO}_4^{\bullet-}$ can be produced by activating PS using various methods, including ultraviolet (UV), heat, ultrasound, transition metal ions (Diao *et al.* 2020; Du *et al.* 2020; Deng *et al.* 2023; Cabrera-Reina *et al.* 2023) and heterogeneous transition metal catalysts (Cai *et al.* 2022; Zhang *et al.* 2023a). The activation of PS by heterogeneous transition metals is independent of additional energy requirements. Additionally, these metals can be easily recovered after the reaction and thus secondary pollution is avoided, which is more favorable in practical applications (Li *et al.* 2022b, Dai *et al.* 2023).

Recently, Fe_3O_4 was frequently applied to PS activation for the removal of organic pollutants due to its excellent magnetism and environmental friendliness (Peng *et al.* 2018). Fe^{2+} had the ability to activate PS and generate more $\text{SO}_4^{\bullet-}$, which was efficient for the degradation of organic pollutants (Zhu *et al.* 2022). Nonetheless, Fe^{2+} on the surface of Fe_3O_4 tended to be oxidized to Fe^{3+} during the activation of PS, and agglomeration was likely to occur among Fe_3O_4 nanoparticles due to their inherent magnetic properties, leading to the reduction of their specific surface area and the efficiency of activating PS (Zhang *et al.* 2022a).

Molybdenum disulfide (MoS_2) was widely utilized in the wastewater treatment due to its low toxicity, abundant active center and high electron mobility (Jlidi *et al.* 2021). It was proved that MoS_2 could be used to activate PS to enhance the degradation of organic pollutants (Wang *et al.* 2021a). Mo^{4+} exposed due to S defect in MoS_2 could be used as an active site to reduce Fe^{3+} to Fe^{2+} , thus promoting the $\text{Fe}^{3+}/\text{Fe}^{2+}$ recycling (Lu *et al.* 2021). Song *et al.* found that MoS_2 could be used as a cocatalyst of Fe^{2+} to activate PS for the degradation of sulfisoxazole (SIX). The regeneration of Fe^{2+} was accelerated because Mo^{4+} in MoS_2 could convert Fe^{3+} to Fe^{2+} , and the removal efficiency of SIX was as high as 97.1% within 40 min

(Song *et al.* 2020a). Kuang *et al.* added MoS₂ into the Fe³⁺/PS system to degrade p-chloroaniline (PCA), and the electron-rich Mo⁴⁺ could transform Fe³⁺ into Fe²⁺ through electron transfer, and thus Fe²⁺ could be continuously produced and continuous degradation of PCA was achieved (Kuang *et al.* 2021). However, the separation and recovery from the solution of MoS₂ could only be performed by repeated filtration or centrifugation, which was a complicated and expensive process.

One possible strategy to solve the above problems is to combine MoS₂ and Fe₃O₄ to prepare a magnetic MoS₂/Fe₃O₄ composite, which can realize rapid separation and recovery of MoS₂ under a magnetic field. Mo⁴⁺ in MoS₂ can promote the Fe³⁺/Fe²⁺ cycle on the surface of Fe₃O₄ and improve its catalytic activity. However, there are few reports on MoS₂/Fe₃O₄ as a PS activator, and the mechanisms are still unclear.

In this study, MoS₂/Fe₃O₄ was prepared as a PS activator by solvothermal hydrothermal method for the effective removal of TC. The structure, morphology and chemical composition of MoS₂/Fe₃O₄ were explored and its catalytic performance for PS was evaluated. Meanwhile, the effects of MoS₂/Fe₃O₄ dosage, PS concentration, initial pH, temperature and common inorganic anions on TC degradation were investigated. The mechanisms of MoS₂/Fe₃O₄ as a PS activator were proposed, the possible degradation pathways of TC in the MoS₂/Fe₃O₄/PS system were revealed, and the risk of TC and its degradation intermediates to aquatic organism were predicted. It is anticipated that MoS₂/Fe₃O₄ can serve as an efficient PS activator for the enhanced degradation of TC and simultaneously be separated and recovered by simple operations.

2. MATERIALS AND METHODS

2.1. Chemicals

Detailed information on chemicals and reagents was shown in the Supporting Materials (Text S1).

2.2. Synthesis of catalysts

2.2.1. Synthesis of Fe₃O₄

Fe₃O₄ was prepared using a solvothermal method (Dolatabadi *et al.* 2023). Specifically, 1.2 g FeCl₃·6H₂O and 0.5 g Na₃C₆H₅O₇·2H₂O were dissolved in 30 mL ethylene glycol (EG) solution at 35 °C by magnetic stirring. Then 3.04 g CH₃COONa was added into the above solution and stirred for 1 h to obtain the precursor. The precursor was poured into a 50 mL Teflon-lined stainless steel autoclave and placed in a constant temperature oven at 200 °C for 12 h. The resulting solid products were collected, washed alternately with deionized water and anhydrous ethanol and then dried in a vacuum drying oven at 55 °C for 10 h to obtain Fe₃O₄ nanoparticles.

2.2.2. Synthesis of MoS₂/Fe₃O₄

First, 1 mmol of (NH₄)₆Mo₇O₂₄·4H₂O was added to 35 mL deionized water by stirring. Different doses of Fe₃O₄ (0.1, 0.15 and 0.2 g) were added and stirred for 30 min. Then, 2.66 g thiourea was added to the above mixture and stirred again for 30 min. The mixture was then transferred into a 50 mL Teflon-lined stainless steel autoclave and placed in a constant temperature oven at 180 °C for 12 h. Then the solid products were collected and washed alternately with deionized water and anhydrous ethanol. After drying at 55 °C for 10 h in a vacuum drying oven, MoS₂/Fe₃O₄ was obtained, which was labeled as FeM-0.1, FeM-0.15, and FeM-0.2 based on the dosage of Fe₃O₄, respectively.

2.3. Characterization

Detailed information on characterization was given in the Supporting Materials (Text S2).

2.4. Experimental procedure

400 mL TC (20 mg·L⁻¹) was added into a 500 mL beaker and placed in a thermostatic water bath (25 °C) for magnetic agitation. The initial pH of the solution was adjusted using 0.1 mol·L⁻¹ HCl or 0.1 mol·L⁻¹ NaOH, and then 4 mmol·L⁻¹ PS and 0.4 g·L⁻¹ MoS₂/Fe₃O₄ were added to initiate the reaction. At an interval of 10 min, a 5 mL aliquot sample was collected and filtered by a 0.22 μm filter. At the same time, the reaction was immediately terminated with 0.5 mL Na₂S₂O₃ (0.1 mol·L⁻¹). After the reaction, MoS₂/Fe₃O₄ was recovered and washed alternately with deionized water and anhydrous ethanol three times. Finally, it was dried under vacuum conditions at 60 °C for the recycling experiment.

2.5. Analysis methods

TC concentration was detected using a UV-visible spectrophotometer (UV-1800, AUCY Scientific, China) at 357 nm (Fatimah *et al.* 2023). The pH meter (Five Easy Plus, Mettler-Toledo, China) was used to determine the pH of the solution. The

inductively coupled plasma spectrometry (ICP, Agilent 700 ICP-OES, USA) was used to detect the concentrations of the leaching metal ions in the liquid in the reaction system. Electron paramagnetic resonance spectroscopy (EPR, Bruker A300, Germany) was used to analyze the active species for TC degradation. The degradation intermediates of TC were identified using a liquid chromatography-mass spectrometer (LC-MS, Waters 2695, USA) and the details are shown in Text S3. The calculation method and data for the Fukui function are presented in Text S4. Details of the degradation intermediates and their toxicity assessment are summarized in Text S5 and Table S3.

2.6. Effect of loading dose of Fe_3O_4 in $\text{MoS}_2/\text{Fe}_3\text{O}_4$ on TC degradation

As presented in Fig. S1, the degradation efficiency of TC was 91.8% in the $\text{MoS}_2/\text{Fe}_3\text{O}_4$ system, while it decreased to 85.5 and 81.1% in the FeM-0.1 and FeM-0.2 systems, respectively. It was reported that the specific surface area and the number of active sites increased with the rising addition of Fe_3O_4 , consequently improving the TC degradation efficiency (Li *et al.* 2023e; Sun *et al.* 2020). However, excessive Fe_3O_4 might cover the reactive active site on the MoS_2 surface and influence the electron transfer (Song *et al.* 2023). As a result, FeM-0.15 was chosen for further investigation, and $\text{MoS}_2/\text{Fe}_3\text{O}_4$ was referred to FeM-0.15 in the following discussion.

3. RESULTS AND DISCUSSION

3.1. Characterization of $\text{MoS}_2/\text{Fe}_3\text{O}_4$

As shown in Figure 1, the peaks located at 18.31° , 30.12° , 35.48° , 43.12° , 57.03° and 62.62° corresponded to (111), (220), (311), (400), (511) and (440) planes of Fe_3O_4 (PDF#75-0033), respectively. The detected diffraction peaks at 14.38° , 32.68° , 33.51° , 39.54° , 49.79° , 58.33° and 60.14° matched with the (002), (100), (101), (103), (105), (110) and (008) crystal planes of MoS_2 (PDF#37-1492), respectively. $\text{MoS}_2/\text{Fe}_3\text{O}_4$ presented the characteristic peaks of MoS_2 and Fe_3O_4 . The absence of individual peaks could be attributed to the low crystallinity of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ (Lu *et al.* 2021), which demonstrated $\text{MoS}_2/\text{Fe}_3\text{O}_4$ was successfully synthesized using a precipitation-hydrothermal method.

Figure 2(a) shows that Fe_3O_4 appeared as uniform spherical nanoparticles with an approximate diameter of 100 nm. In Figure 2(b), MoS_2 presented a flower-like microsphere structure assembled from nanosheets of different dimensions, and its average diameter was about 5 μm . Figure 2(c) shows that Fe_3O_4 nanoparticles were uniformly attached on the surface of MoS_2 to form $\text{MoS}_2/\text{Fe}_3\text{O}_4$, which could effectively avoid the agglomeration of Fe_3O_4 nanoparticles. As present in Figure 2(d), the MoS_2 nanofakes and Fe_3O_4 nanoparticles were observed, and Fe_3O_4 nanoparticles were embedded into the nanofakes of MoS_2 . Figure 2(e) displays that two distinct lattice fringes were observed in the HRTEM image of $\text{MoS}_2/\text{Fe}_3\text{O}_4$. The fringes with lattice spacing of 0.210 and 0.274 nm corresponded to the (400) planes of Fe_3O_4 and (100) planes of MoS_2 , respectively (Yi *et al.* 2021; Yu *et al.* 2022).

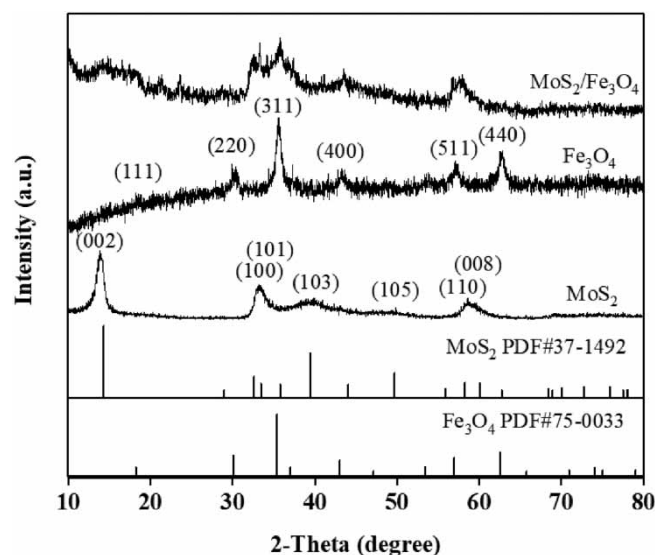


Figure 1 | XRD pattern of $\text{MoS}_2/\text{Fe}_3\text{O}_4$.

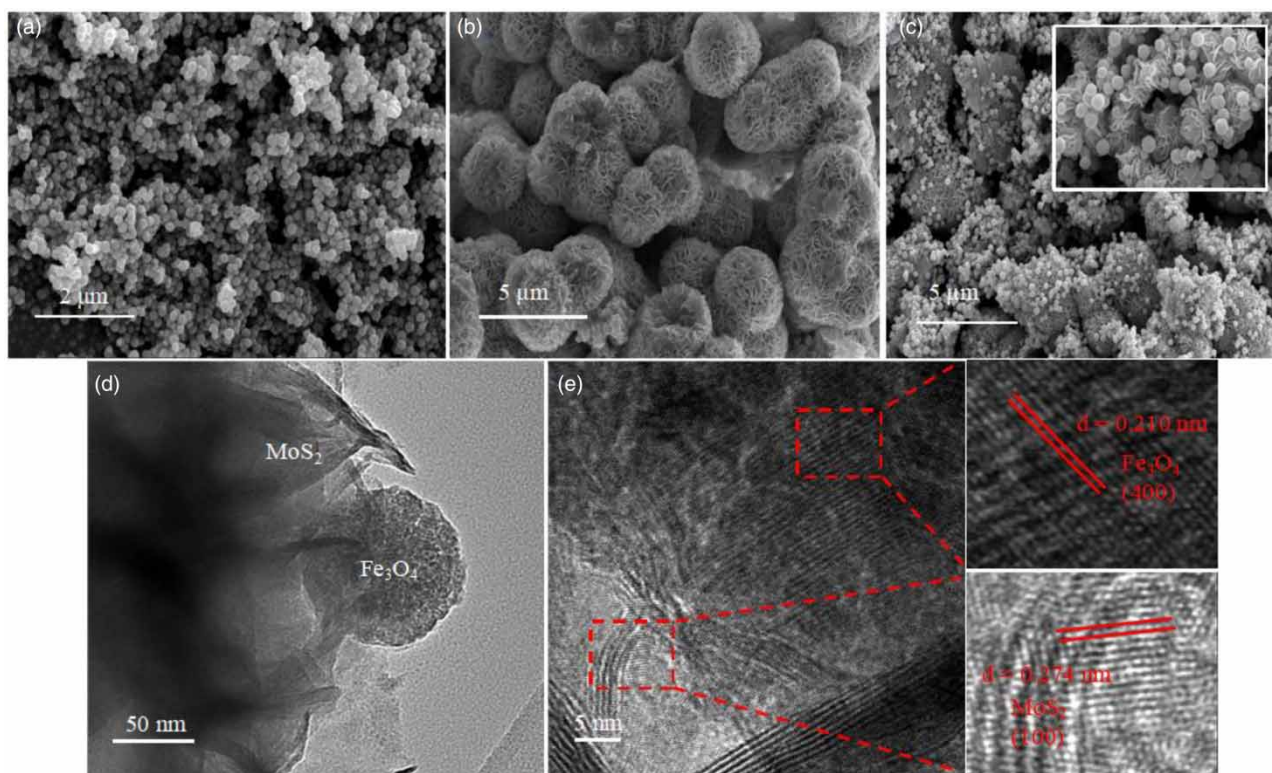


Figure 2 | (a) SEM image of Fe_3O_4 ; (b) SEM image of MoS_2 ; (c) SEM image of $\text{MoS}_2/\text{Fe}_3\text{O}_4$; (d) TEM image of $\text{MoS}_2/\text{Fe}_3\text{O}_4$; (e) HRTEM image of $\text{MoS}_2/\text{Fe}_3\text{O}_4$.

As shown in Figure 3(a), only Mo, S, Fe and O elements were observed on the surface of $\text{MoS}_2/\text{Fe}_3\text{O}_4$, with an atomic ratio of Fe/Mo of 1:1.5. EDS element mapping (Figure 3(b)–3(f)) revealed that Mo, S, Fe and O elements were uniformly distributed, further affirming that Fe_3O_4 were successfully anchored on MoS_2 and thus achieved favorable PS activation. Additionally, Guo *et al.* (2023) also demonstrated that better dispersity provided more active sites on the surface of the composite, contributing to the synergistic effect between MoS_2 and Fe_3O_4 and PS activation.

As shown in Figure 4(a), the peaks detected at 710.6 and 724.3 eV corresponded to $\text{Fe}^{2+} 2p_{3/2}$ and $\text{Fe}^{2+} 2p_{1/2}$, respectively, while the peaks at 713.1 and 727.1 eV were attributed to $\text{Fe}^{3+} 2p_{3/2}$ and $\text{Fe}^{3+} 2p_{1/2}$, respectively. The peaks located at 719.1 and 733.3 eV were satellite peaks of $\text{Fe} 2p_{3/2}$ and $\text{Fe} 2p_{1/2}$, respectively (Huang *et al.* 2019; Tong *et al.* 2022). The two typical peaks at 228.5 and 231.8 eV in Figure 4(b) were assigned to $\text{Mo}^{4+} 3d_{5/2}$ and $\text{Mo}^{4+} 3d_{3/2}$, respectively (Li *et al.* 2022c). A weak peak at 235.3 eV was ascribed to Mo^{6+} because negligible MoS_2 was oxidized into MoO_3 . The peaks at 229.5 and 232.80 eV corresponded to $\text{Mo}^{5+} 3d_{5/2}$ and $\text{Mo}^{5+} 3d_{3/2}$ of MoS_2 . A peak detected at 225.6 eV was attributed to S 2s of MoS_2 . In the O 1s spectra of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ (Figure 4(c)), two peaks located at 530.2 and 531.7 were defined as the lattice oxygen in metal oxides (M-O) and surface hydroxyl group (-OH), respectively (Huang *et al.* 2019). For the S 2p spectra of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ (Figure 4(d)), the peaks at 161.4 and 162.7 eV were assigned to S $2p_{3/2}$ and S $2p_{1/2}$, respectively (Luo *et al.* 2021a). Based on the above characteristics, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ had been successfully synthesized.

The recovery of the magnetic compounds was simple, which could reduce the operating costs and the secondary pollution (Fernández-Velayos *et al.* 2022; Swami *et al.* 2023). As shown in Figure 5, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ exhibited superparamagnetism with a saturation magnetization of 9.73 emu g^{-1} . In addition, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ could be separated from the solution within 120 s under the action of the magnet as shown in Figure 5, avoiding its unnecessary loss (Wang *et al.* 2021b).

3.2. TC degradation

3.2.1. PS activation performance of $\text{MoS}_2/\text{Fe}_3\text{O}_4$

As shown in Figure 6(a), only 6.1% of TC could be removed within 60 min in a single PS system, while 15.2% when $\text{MoS}_2/\text{Fe}_3\text{O}_4$ was used due to the limited adsorption of TC by $\text{MoS}_2/\text{Fe}_3\text{O}_4$. The removal efficiencies of TC in the $\text{Fe}_3\text{O}_4/\text{PS}$ and

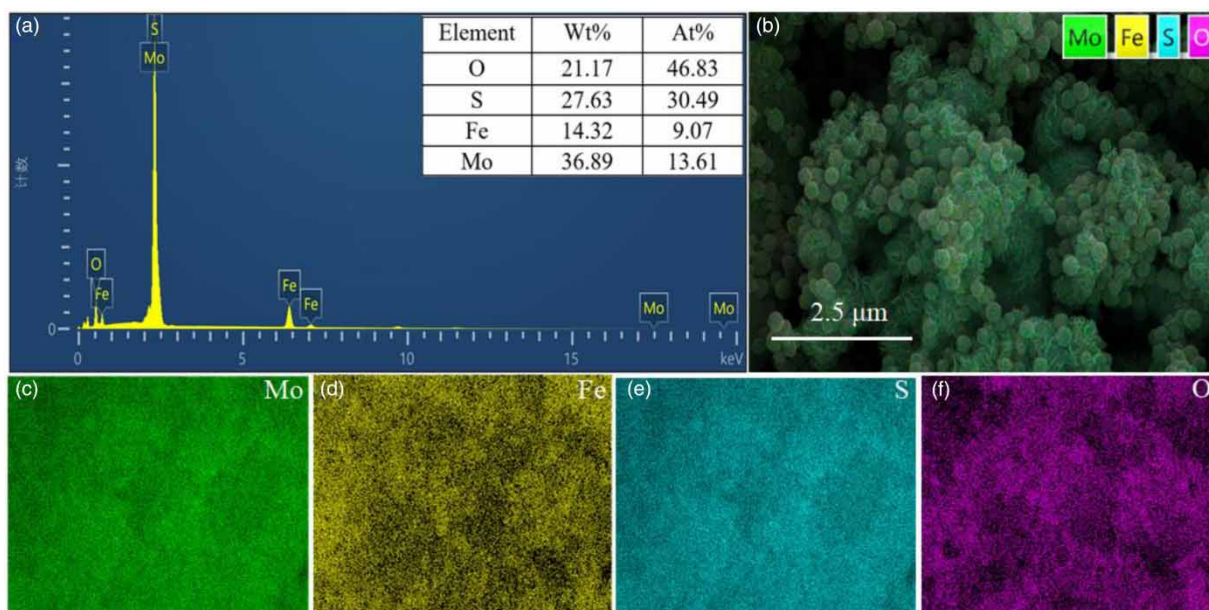


Figure 3 | (a) EDS pattern of $\text{MoS}_2/\text{Fe}_3\text{O}_4$; (b–f) EDS element mapping of Mo, Fe, O and S of $\text{MoS}_2/\text{Fe}_3\text{O}_4$.

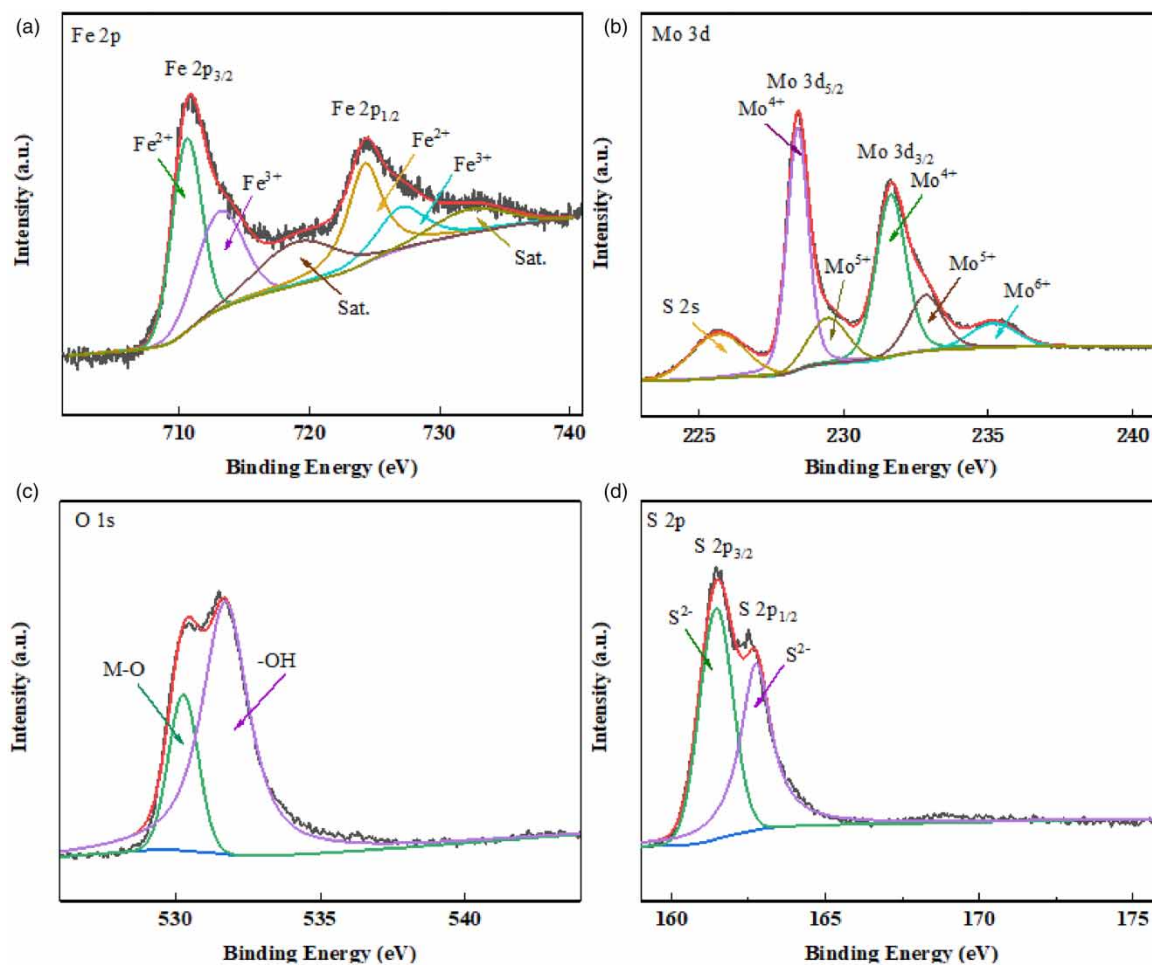


Figure 4 | XPS spectra of the $\text{MoS}_2/\text{Fe}_3\text{O}_4$: (a) Fe 2p, (b) Mo 3d, (c) O 1s and (d) S 2p.

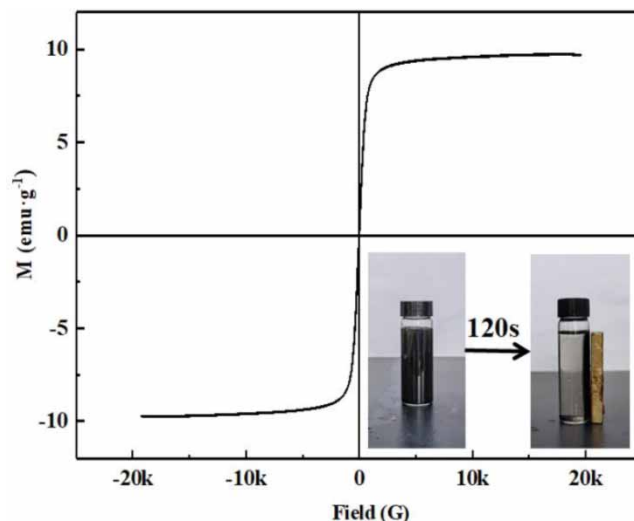


Figure 5 | M - H curve of $\text{MoS}_2/\text{Fe}_3\text{O}_4$.

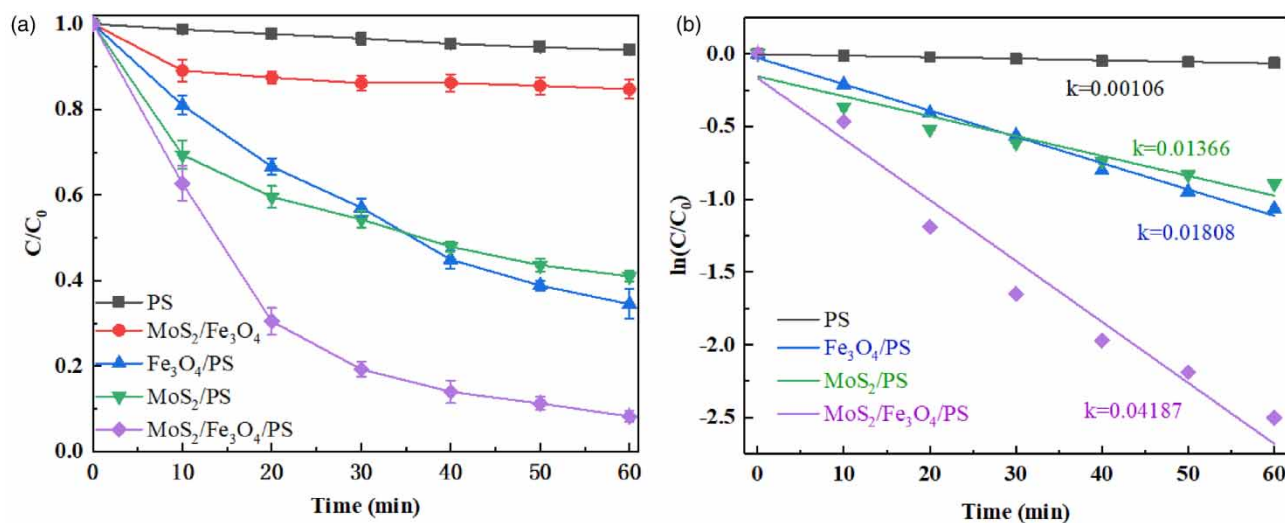


Figure 6 | (a) Removal efficiency of TC in various systems. (b) Kinetics of TC degradation. Reaction conditions: $[\text{MoS}_2/\text{Fe}_3\text{O}_4] = 0.4 \text{ g}\cdot\text{L}^{-1}$, $[\text{PS}] = 4 \text{ mmol}$, $[\text{TC}] = 20 \text{ mg}\cdot\text{L}^{-1}$, initial $\text{pH} = 7$, $T = 25^\circ\text{C}$ and reaction time = 60 min.

MoS_2/PS systems were 65.5 and 59%, respectively. These results showed that a single Fe_3O_4 or single MoS_2 was invalid in activating PS to degrade TC. However, in the $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ system, the removal efficiency of TC was significantly improved to 91.8% after 60 min reaction, which was much higher than the $\text{Fe}_3\text{O}_4/\text{PS}$ or MoS_2/PS systems as there might be a synergistic effect between MoS_2 and Fe_3O_4 for PS activation. The degradation of TC followed the first-order reaction kinetic model ($R^2 > 0.92$), as shown in Figure 6(b). The reaction rate constant (k_{obs}) values for PS, $\text{Fe}_3\text{O}_4/\text{PS}$, MoS_2/PS and $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ systems were 0.00106, 0.01808, 0.01366 and 0.04187 min^{-1} , respectively. The k_{obs} values of the $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ system were 39.5, 2.32 and 3.06 times higher than those of PS, $\text{Fe}_3\text{O}_4/\text{PS}$ and MoS_2/PS systems, respectively. As shown in Table 1, compared with similar studies, we used the hydrothermal method to load Fe_3O_4 nanoparticles onto MoS_2 of flower-shaped microspheres, avoiding the aggregation of Fe_3O_4 nanoparticles and accelerating the surface $\text{Fe}^{3+}/\text{Fe}^{2+}$ cycling. The preparation method was simple and a small amount of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ could effectively degrade TC in a short time. In summary, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ exhibited efficient catalytic ability for TC degradation.

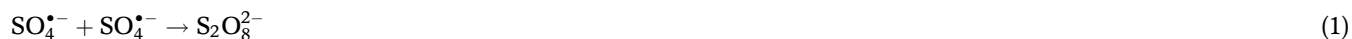
Table 1 | Comparison of this work with previous reports on the use of different catalysts to degrade TC

Catalyst	Preparation method	Structure	Dosage (g·L ⁻¹)	TC (mg·L ⁻¹)	Reaction time (min)	Removal efficiency (%)	Reference
Fe ₃ O ₄	Commercial purchase	Nanoparticles	1	100	90	89.0	Hou <i>et al.</i> (2012)
Fe ₃ O ₄ @JDC	Soaking and calcination method	Nanoparticles anchored on the surface of tubular JDC	0.1	10	60	90.2	Zhang <i>et al.</i> (2023c)
BC300-MoS ₂ -1	Hydrothermal method	Flower-like cluster framework	0.05	20	120	78	Su <i>et al.</i> (2022)
FeOOH@MoS ₂	Hydrothermal-chemical deposition method	Nanosheet structure	0.4	50	30	85	Yi <i>et al.</i> (2021)
Fe ₃ O ₄ /CoS ₂	Hydrothermal method	Regular polyhedron	0.1	20	20	88.3	Qiu <i>et al.</i> (2024)
C@Fe ₃ O ₄	One-pot hydrothermal method	Hollow sphere structure	0.5	100	90	78.5	Peng <i>et al.</i> (2018)
CoFe ₂ O ₄ @MoS ₂	One-pot hydrothermal method	Nanoparticles distributed in the MoS ₂ flakes	0.2	10	30	80.4	Peng <i>et al.</i> (2022)
Fe ₃ O ₄ /MoS ₂	Hydrothermal method	Nanoparticles attached on the surface of MoS ₂	0.4	20	60	91.8	This work

3.2.2. Effects of MoS₂/Fe₃O₄ dosage and PS concentration

As the dosage was increased from 0.1 to 0.4 g·L⁻¹, the removal efficiency of TC improved from 61.3 to 91.8% (Figure 7(a)), which could be attributed to the increase of reactive sites for PS activation with higher MoS₂/Fe₃O₄ dosage (Yi *et al.* 2021). However, when the dosage was increased to 0.5 g·L⁻¹, the removal efficiency of TC only increased by 1.5%, which suggested that excessive MoS₂/Fe₃O₄ addition could not facilitate TC removal as PS was insufficient. Therefore, 0.5 g·L⁻¹ MoS₂/Fe₃O₄ was selected for further experiments.

In Figure 7(b), as the PS concentration was increased from 1.0 to 4.0 mmol·L⁻¹, the removal efficiency of TC elevated from 46.3 to 91.8%. When the PS concentration was further increased from 4.0 to 5.0 mmol·L⁻¹, the degradation efficiency of TC decreased from 91.8 to 86.9%. It was inferred that the generation rate of free radicals increased with the rising PS concentration, thus enhancing the removal efficiency of TC (Li *et al.* 2023a; Sun *et al.* 2020). However, excessive PS inhibited the degradation of TC because the increased SO₄^{•-} was quenched by itself or PS through the following equations (Li *et al.* 2022c; Liu *et al.* 2022a).



3.2.3. Effects of pH and temperature

At initial pH values of 3, 5 and 7, the removal efficiencies of TC were 94.8, 93.5 and 91.8%, respectively. However, at initial pH values of 9 and 10, the removal efficiencies of TC decreased to 84.2 and 42.9%, respectively (Figure 7(c)). It was thus inferred that the favorable TC degradation in the MoS₂/Fe₃O₄/PS system could be achieved within the initial pH range of 3–7. The pH in the MoS₂/Fe₃O₄/PS system was monitored during the reaction, as shown in Figure S2. When initial pH values were 3, 5 and 7, the pH dropped below 3.30 after 10 min and continued to decrease in subsequent reactions. When initial pH values were 9 and 10, the pH remained above 3.89 within 60 min. The zero charge point (pH_{PZC}) of the MoS₂/Fe₃O₄ surface was approximately 3.66 (Figure 7(d)). Therefore, the MoS₂/Fe₃O₄ surface carried positive charges after 10 min at initial pH values lower than 7, and S₂O₈²⁻ with negative charges was easily adsorbed on the surface of MoS₂/Fe₃O₄, which promoted the activation of PS and improved the removal efficiency of TC (Zhu *et al.* 2022). However, the MoS₂/Fe₃O₄ surface carried negative charges within 60 min at initial pH values higher than 9, and the electrostatic repulsion prevented the contact between MoS₂/Fe₃O₄ and PS, inhibiting the degradation of TC (Luo *et al.* 2021b).

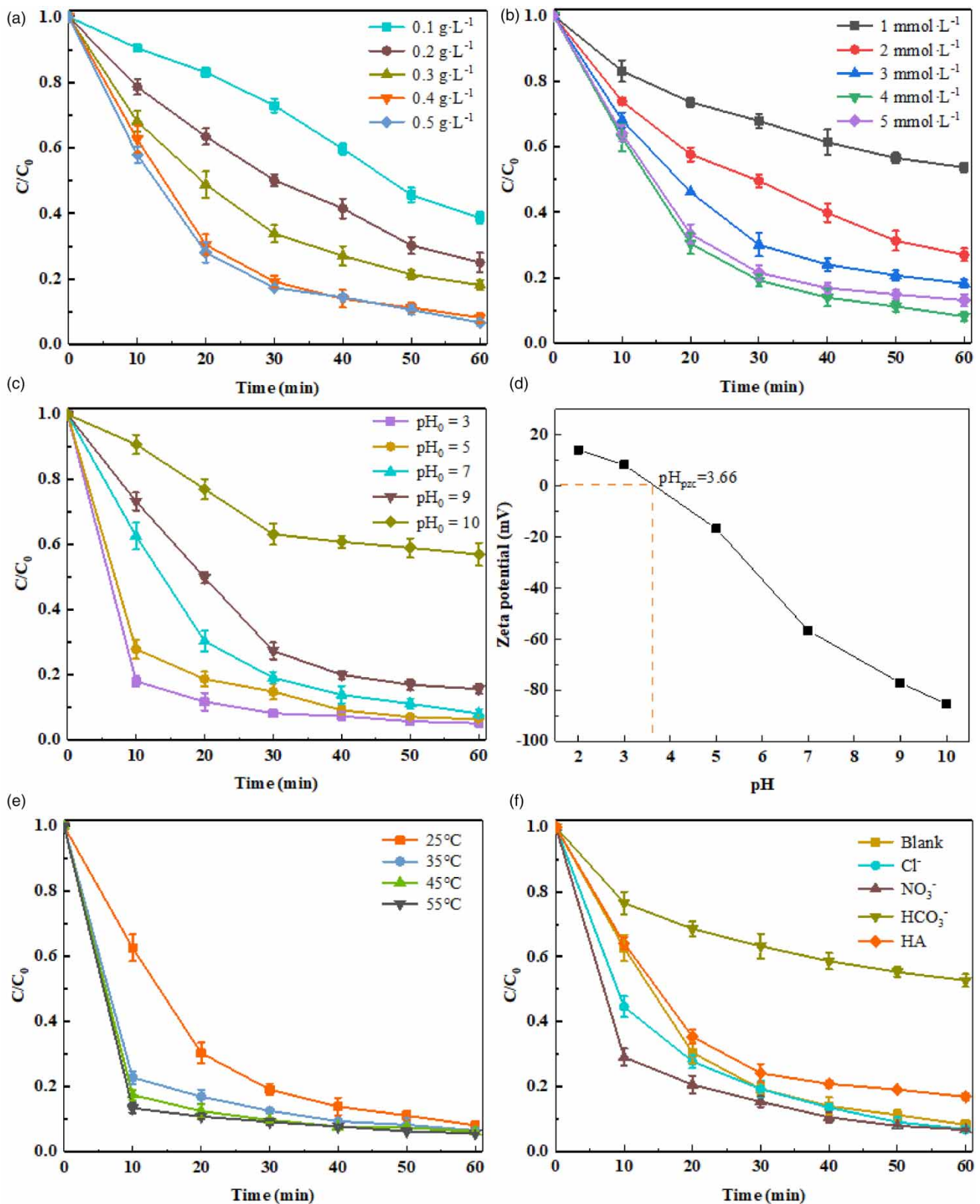


Figure 7 | Effects of reaction parameters on the TC degradation: (a) the dosage of $\text{MoS}_2/\text{Fe}_3\text{O}_4$; (b) PS concentration; (c) initial pH; (d) Zeta potential of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ at different pH values; (e) temperature; (f) inorganic anions (Cl^- , NO_3^- , HCO_3^-) and HA. Reaction conditions: $[\text{MoS}_2/\text{Fe}_3\text{O}_4] = 0.4 \text{ g}\cdot\text{L}^{-1}$, $[\text{PS}] = 4 \text{ mmol}$, $[\text{TC}] = 20 \text{ mg}\cdot\text{L}^{-1}$, initial $\text{pH} = 7$, $T = 25 \text{ }^{\circ}\text{C}$ and reaction time = 60 min.

The effect of temperature on TC degradation in the MoS₂/Fe₃O₄/PS system is shown in Figure 7(e). When the temperature was increased from 25 to 35 °C, the removal efficiencies of TC were higher than 90% after 40 min. When the temperature raised to 45 and 55 °C, the removal efficiency reached 90% after 30 min. It indicated that the elevated temperature could accelerate TC degradation in the MoS₂/Fe₃O₄/PS system. Elevated temperature was conducive to the thermal decomposition of PS, promoting the generation of SO₄^{•-} (Guo *et al.* 2016; Zhang *et al.* 2022b).

3.2.4. Effects of inorganic anions and humic acid

The effects of common inorganic anions (Cl⁻, NO₃⁻ and HCO₃⁻) and humic acid (HA) on TC degradation were investigated at a concentration of 3 mmol·L⁻¹. As shown in Figure 7(f), when 3 mmol·L⁻¹ Cl⁻ and NO₃⁻ were added into the MoS₂/Fe₃O₄/PS system, the removal efficiency of TC increased from 37.5 to 55.4 and 70.1% after 10 min, and from 91.8 to 93.2 and 93.4% after 60 min, respectively, demonstrating that the introduction of Cl⁻ and NO₃⁻ accelerated the degradation of TC in the MoS₂/Fe₃O₄/PS system. Cl⁻ could react with SO₄^{•-} to generate Cl[•] and Cl₂^{•-}, and NO₃⁻ could be oxidized by SO₄^{•-} to produce NO₃[•] (Equations (3)–(5)) (Sun *et al.* 2020; Li *et al.* 2023d; Wang *et al.* 2023). Although the oxidation potential of Cl[•], Cl₂^{•-} and NO₃[•] was slightly lower than that of SO₄^{•-}, they could compensate for the depletion of SO₄^{•-} due to Cl⁻ and NO₃⁻ scavenging and enhance the degradation efficiency of TC, which was consistent with previous reports (Song *et al.* 2020a, 2020b). The removal efficiency of TC decreased from 91.8 to 47.3% after 60 min in the presence of HCO₃⁻. This was due to the fact that a part of SO₄^{•-} was quenched by HCO₃⁻ and CO₃²⁻ generated by its ionization (Equations (6) and (7)) (Sun *et al.* 2020; Li *et al.* 2023b). The removal efficiency of TC decreased from 91.8 to 83.2% after adding 3 mmol·L⁻¹ HA into the MoS₂/Fe₃O₄/PS system, indicating that HA suppressed TC degradation. Previous studies had shown that HA could act as a free radical quencher by competing with •OH and SO₄^{•-}. In addition, the phenolic hydroxyl and carboxyl groups in HA were adsorbed on the surface of MoS₂/Fe₃O₄, blocking the active site and hindering the activation of PS (Li *et al.* 2019).



3.3. Mechanisms

3.3.1. EPR testing and quenching experiment

The active species generated in the MoS₂/Fe₃O₄/PS system were identified by EPR testing (Sun *et al.* 2022). As shown in Figure 8(a), no signals were observed in the PS system. In contrast, a DMPO•OH characteristic signal with a peak intensity of 1:2:2:1 was detected in the MoS₂/Fe₃O₄/PS system. This indicated that MoS₂/Fe₃O₄ could effectively activate PS to produce •OH. A DMPO – SO₄^{•-} signal formed by DMPO and SO₄^{•-} was also observed in the MoS₂/Fe₃O₄/PS system. The signal intensity of DMPO – SO₄^{•-} was much weaker than that of DMPO•OH, which was attributed to the fact that SO₄^{•-} could react quickly with H₂O to convert into •OH through Equation (8) (Li *et al.* 2022a). In addition, DMPO and TEMP were applied to capture •O₂⁻ and ¹O₂. Figure 8(b) and 8(c) showed the characteristic signals of DMPO–•O₂⁻ and TEMP-¹O₂, indicating the generation of •O₂⁻ and ¹O₂. The Fe²⁺ on MoS₂/Fe₃O₄ surface could provide an electron for dissolved oxygen to produce •O₂⁻ (Equation (9)), which was consistent with the research results reported by He *et al.* (2021) and Huang *et al.* (2021). Subsequently, the generated •O₂⁻ could interact or react with •OH to generate ¹O₂ (Equations (10) and (11)) (Li *et al.* 2019). Moreover, Mo⁶⁺ on MoS₂/Fe₃O₄ surface could react with •O₂⁻ to produce ¹O₂ (Equation (12)) (Zhang *et al.* 2020). The results of the EPR testing confirmed the presence of SO₄^{•-}, •OH, •O₂⁻ and ¹O₂ in the MoS₂/Fe₃O₄/PS system.

To verify the above conclusions, methanol (MeOH) was used as a quencher for SO₄^{•-} and •OH, while tert-butanol (TBA); ascorbic acid (AA); L-histidine (L-H) were used as quenchers for •OH, •O₂⁻ and ¹O₂, respectively (Li *et al.* 2022c; Peng *et al.* 2022; Liao *et al.* 2011). The removal efficiency of TC decreased from 91.8 to 61.8 and 73.6% with the addition of 1 mol MeOH and TBA, respectively (Figure 8(d)) (Li *et al.* 2022a; Peng *et al.* 2022). The results indicated the presence of •OH and SO₄^{•-} in the MoS₂/Fe₃O₄/PS system, and the contribution of •OH to TC degradation was higher than that of SO₄^{•-}. However, MeOH or TBA did not completely inhibit the degradation of TC, indicating the presence of other active species in the

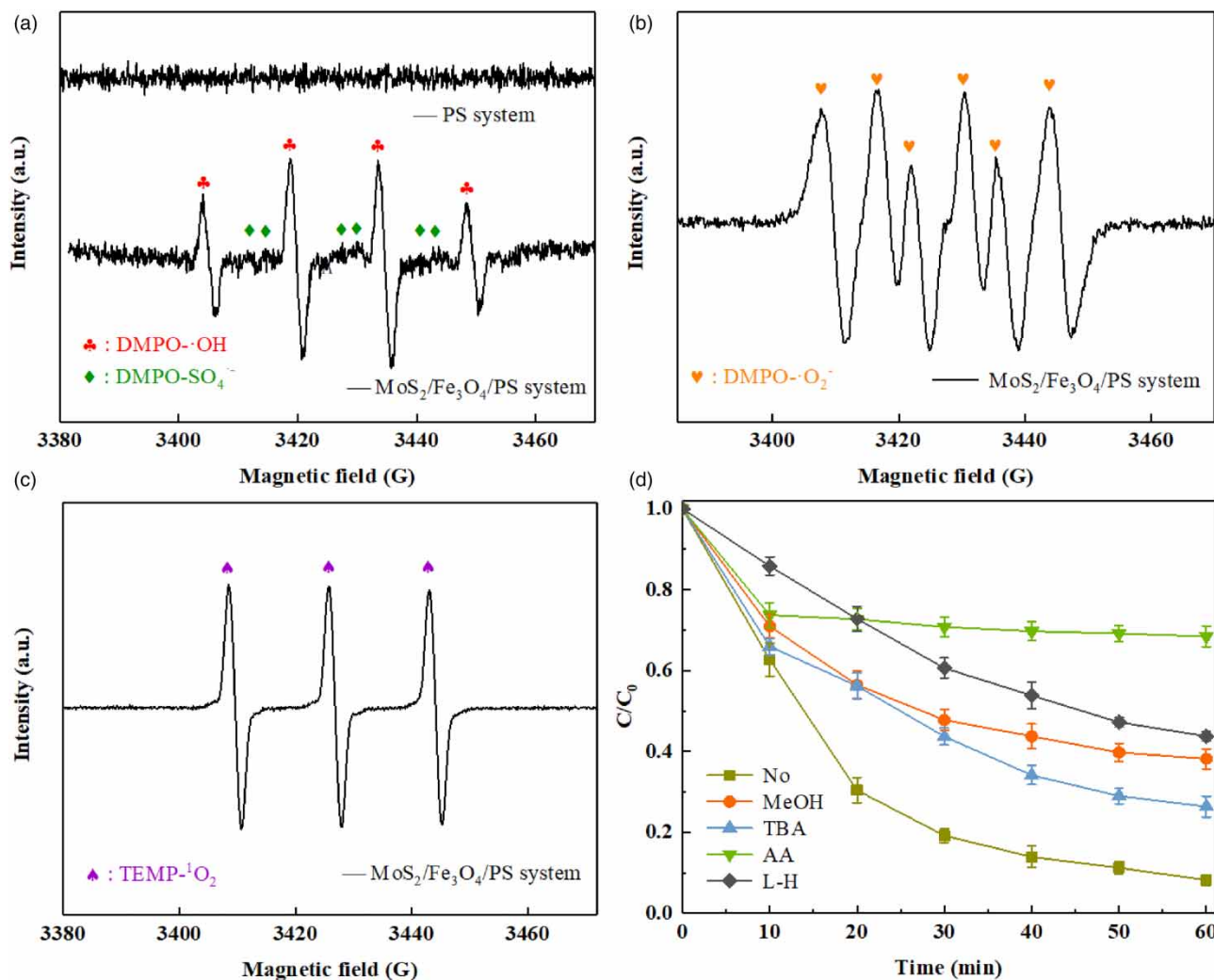


Figure 8 | (a–c) EPR spectrum in the MoS₂/Fe₃O₄/PS system; (d) Effects of radical scavengers on the degradation of TC. Reaction conditions: [MoS₂/Fe₃O₄] = 0.4 g·L⁻¹, [PS] = 4 mmol, [TC] = 20 mg·L⁻¹, initial pH = 7, T = 25 °C and reaction time = 60 min.

MoS₂/Fe₃O₄/PS system. When 10 mmol AA and L-H were added into the MoS₂/Fe₃O₄/PS system, the removal efficiency of TC decreased from 91.8 to 31.5 and 56.3%, respectively, confirming that •O₂⁻ and ¹O₂ also played an important role in TC degradation (Yang *et al.* 2020, 2022), which was consistent with the EPR test results. According to the results of EPR testing and quenching experiments, SO₄^{•-}, •OH, •O₂⁻ and ¹O₂ were present in the MoS₂/Fe₃O₄/PS system, and •OH, •O₂⁻ and ¹O₂ were the predominant active species.



3.3.2. XPS analysis

In order to reveal the mechanism of MoS₂/Fe₃O₄ activating PS, XPS was used to analyze its surface element valence before and after the activation reaction (Figure 9). As shown in Figure 9(a), the proportion of surface Fe³⁺ decreased from 44.7 to 40.4%,

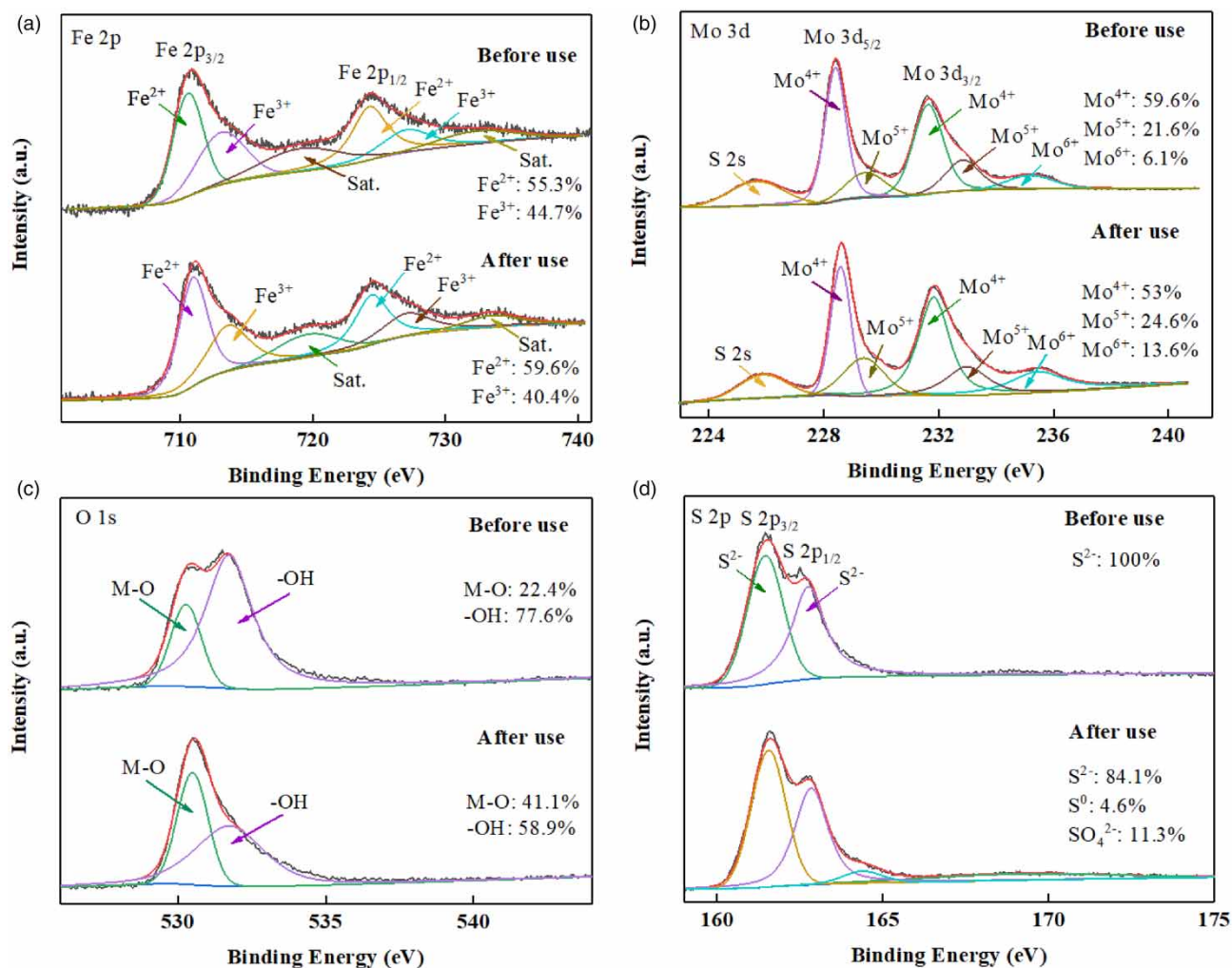


Figure 9 | XPS spectra of MoS₂/Fe₃O₄ before and after use: (a) Mo 3d; (b) Fe 2p; (c) O 1s; (d) S 2p.

while that of Fe²⁺ increased from 55.3 to 59.6% after the activation reaction as a part of Fe³⁺ was reduced to Fe²⁺. Previous reports had shown that Mo⁴⁺ contributed to the regeneration of Fe²⁺ and thus accelerated the cycling of Fe³⁺/Fe²⁺ (Lu *et al.* 2021). Therefore, Fe²⁺ was first oxidized into Fe³⁺ by PS, and then the exposed Mo⁴⁺ continuously reduced Fe³⁺ to Fe²⁺, resulting in an increase of Fe²⁺ proportion. The regeneration of Fe²⁺ was a key step in efficient PS activation and the regenerated Fe²⁺ could participate again in the activation of PS and promote the generation of free radicals. As shown in Figure 9(b), the proportion of Mo⁴⁺ decreased from 59.6 to 53%, and the proportion of Mo⁶⁺ increased from 6.1 to 13.6%, which demonstrated that a portion of Mo⁴⁺ was oxidized into Mo⁶⁺. As shown in Figure 9(c), the proportion of M-O increased from 22.4 to 41.1% after the reaction, which might be due to the production of molybdenum oxide on the catalyst surface. The proportion of surface -OH decreased from 77.6 to 58.9% after the reaction, indicating that the surface -OH of the catalyst also participated in the reaction. In addition, two new peaks appeared at 163.4 and 169.0 eV after the reaction (Figure 9(d)), indicating the formation of S⁰ and SO₄²⁻ on the catalyst surface (Fan *et al.* 2018). This was due to the oxidation of S²⁻ by PS during the reaction process. These results confirmed that Fe₃O₄ and MoS₂ had synergistic effects on PS activation and Mo⁴⁺ in MoS₂/Fe₃O₄ could reduce Fe³⁺ to Fe²⁺, promoting the cycling of Fe³⁺/Fe²⁺ and the production of active species.

3.3.3. Mechanisms of MoS₂/Fe₃O₄ activating PS

Based on the active species identification and XPS analysis, the mechanisms for the PS activation by CuS/Fe₃O₄ were proposed. Firstly, Mo⁴⁺ and Fe²⁺ on the surface of MoS₂/Fe₃O₄ acted as the active sites to activate PS and produce SO₄^{•-}

(Equations (13) and (14)). The generated $\text{SO}_4^{\bullet-}$ was further converted to $\bullet\text{OH}$ (Equation (15)), and Mo^{4+} and Fe^{2+} were oxidized to Mo^{6+} and Fe^{3+} , respectively. Fe^{2+} on the surface of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ reacted with dissolved oxygen to form $\bullet\text{O}_2^-$, and $\bullet\text{O}_2^-$ was further converted to $^1\text{O}_2$ by self-reaction or reacting with $\bullet\text{OH}$ (Equations (9)–(11)). In addition, Mo^{6+} on $\text{MoS}_2/\text{Fe}_3\text{O}_4$ surface could react with $\bullet\text{O}_2^-$ to produce $^1\text{O}_2$ (Equation (12)). Mo^{4+} could be used as an electron donor to reduce Fe^{3+} to Fe^{2+} (Equation (16)). This process promoted the cycle of $\text{Fe}^{3+}/\text{Fe}^{2+}$ and ensured sufficient Fe^{2+} on the surface of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ to improve the catalytic activity of $\text{MoS}_2/\text{Fe}_3\text{O}_4$.



3.3.4. TC degradation pathway and toxicity assessment

Fukui index was employed to analyze the main sites for reactive species on TC molecule on the basis of the Density functional theory (DFT) calculation (Cheng & Ji 2022; Wu *et al.* 2022). In this study, $\text{SO}_4^{\bullet-}$, $\bullet\text{OH}$, $\bullet\text{O}_2^-$ and $^1\text{O}_2$ were the attack species participated in TC degradation in the $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ system. Therefore, f^- and f^0 were taken into account to predict the active site of TC in the degradation process (Chen *et al.* 2023). Fukui index (f^0 , f^+ and f^-) and the Natural Population Analysis (NPA) charges distribution are shown in Table S1, and the optimized structure of TC is listed in Fig. S3. Generally, the Fukui exponent values with larger f^- and f^0 were more likely to be attacked by $^1\text{O}_2$ and free radicals ($\text{SO}_4^{\bullet-}$, $\bullet\text{OH}$, $\bullet\text{O}_2^-$), respectively (Cheng & Ji 2022). Hence, N14 (0.0581) and C7 (0.0751) with higher f^- was susceptible to $^1\text{O}_2$ attack. C7 (0.0455) and C12 (0.0401) with larger f^0 values were vulnerable reaction sites for $\text{SO}_4^{\bullet-}$, $\bullet\text{OH}$, $\bullet\text{O}_2^-$ attack, which could undergo oxidation, hydroxylation, and double bond breaking (Zhang *et al.* 2023b). Although C12 had a larger f^0 value, the attack of free radicals was difficult because of the saturated sites and steric hindrance (Wu *et al.* 2023).

According to the detected intermediates (Table S2) and the Fukui index, the possible degradation pathways of TC in the $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ system are shown in Figure 10. In path I, C7 was attacked by $\text{SO}_4^{\bullet-}$, $\bullet\text{OH}$, $\bullet\text{O}_2^-$ and $^1\text{O}_2$ and TC was

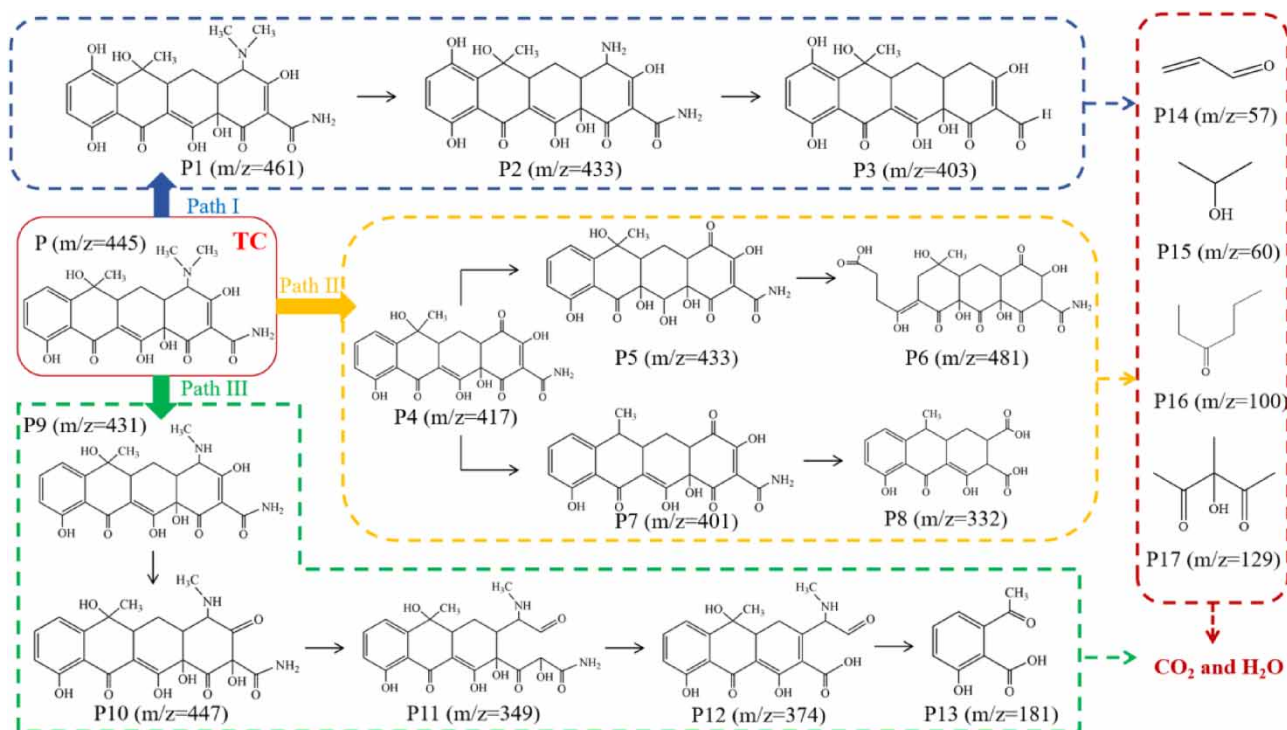


Figure 10 | Degradation pathway of TC.

hydroxylated to produce P1 ($m/z = 461$). P2 ($m/z = 309$) was also formed due to the loss of two dimethyl from P1, and then P2 was converted into P3 ($m/z = 213$) owing to the loss of two amino groups (Wang *et al.* 2017). In path II, N14 tended to be attacked by $^1\text{O}_2$ because of its relative larger f^- (0.0581) value. The dimethylamino in the TC was oxidized to the ketone group to form P4 ($m/z = 417$). P4 was hydroxylated to produce P5 ($m/z = 433$). P5 was further oxidized, causing the fracture of the aromatic ring to produce P6 ($m/z = 481$). In addition, P7 ($m/z = 401$) was formed by the dehydration of P4, and P7 was further oxidized by free radicals to form P8 ($m/z = 332$) (Pi *et al.* 2019). In path III, TC was transformed into P9 ($m/z = 431$) owing to the C-N cleavage and dehylation. P10 ($m/z = 447$) was generated owing to the hydroxylation of P9 and could be further oxidized to P11 ($m/z = 349$) by free radicals. P12 ($m/z = 374$) was stemmed from subsequent deamidation of P11 ($m/z = 349$), and was further opened in the ring to produce P13 ($m/z = 181$) (Guo *et al.* 2023). P3, P6, P8 and P13 was further degraded into small organic molecules including P14 ($m/z = 57$), P15 ($m/z = 60$), P16 ($m/z = 100$) and P17 ($m/z = 129$) (Dong *et al.* 2022). Eventually, these short-chain organic molecules were oxidized and decomposed into H_2O and CO_2 .

Furthermore, ECOSAR software was applied to predict the toxicity of TC and its intermediate products (Yin *et al.* 2018). The toxicity values for fish LC50 (96 h), daphnid LC50 (48 h) and green algae EC50 (48 h) are presented in Table S3 and the range of toxicity values is shown in Table S4. As demonstrated in Figure 11, the acute toxicity values for fish and green algae were calculated as 61.44 and 17.68 $\text{mg}\cdot\text{L}^{-1}$, which was 'harmful'. The value for daphnid was 4.49 $\text{mg}\cdot\text{L}^{-1}$ in the 'toxic' range. The chronic toxicity value for fish was 0.96 $\text{mg}\cdot\text{L}^{-1}$, which was classified as 'very toxic'. The values for daphnid and green algae were 1.04 and 2.52 $\text{mg}\cdot\text{L}^{-1}$, which indicated that TC had a certain toxic effect on aquatic organisms. It was worth noting that P3 and P9 were 6.29 and 12.12 $\text{mg}\cdot\text{L}^{-1}$, which indicated the slightly higher toxicity to green algae than TC. However, as the oxidation reaction occurred, toxicity values of other intermediates were lower than that of TC, which fell in the 'no harmful' or 'harmful' range, indicating that the $\text{MoS}_2/\text{Fe}_3\text{O}_4$ system could not only effectively degrade TC, but also reduce certain toxic effects.

3.3.5. Recyclability and stability of $\text{MoS}_2/\text{Fe}_3\text{O}_4$

As shown in Figure 12(a), after three recycles, the degradation efficiency of TC was still higher than 86% after 60 min, which proved that the $\text{MoS}_2/\text{Fe}_3\text{O}_4$ had excellent recyclability. The slight decrease of TC degradation efficiency during the recycle experiment might be due to the adsorption of TC degradation intermediates on $\text{MoS}_2/\text{Fe}_3\text{O}_4$ surface, leading to the plugging of active sites (Sun *et al.* 2020; Li *et al.* 2023c). In addition, the reduction of the proportion of Mo^{4+} on the $\text{MoS}_2/\text{Fe}_3\text{O}_4$

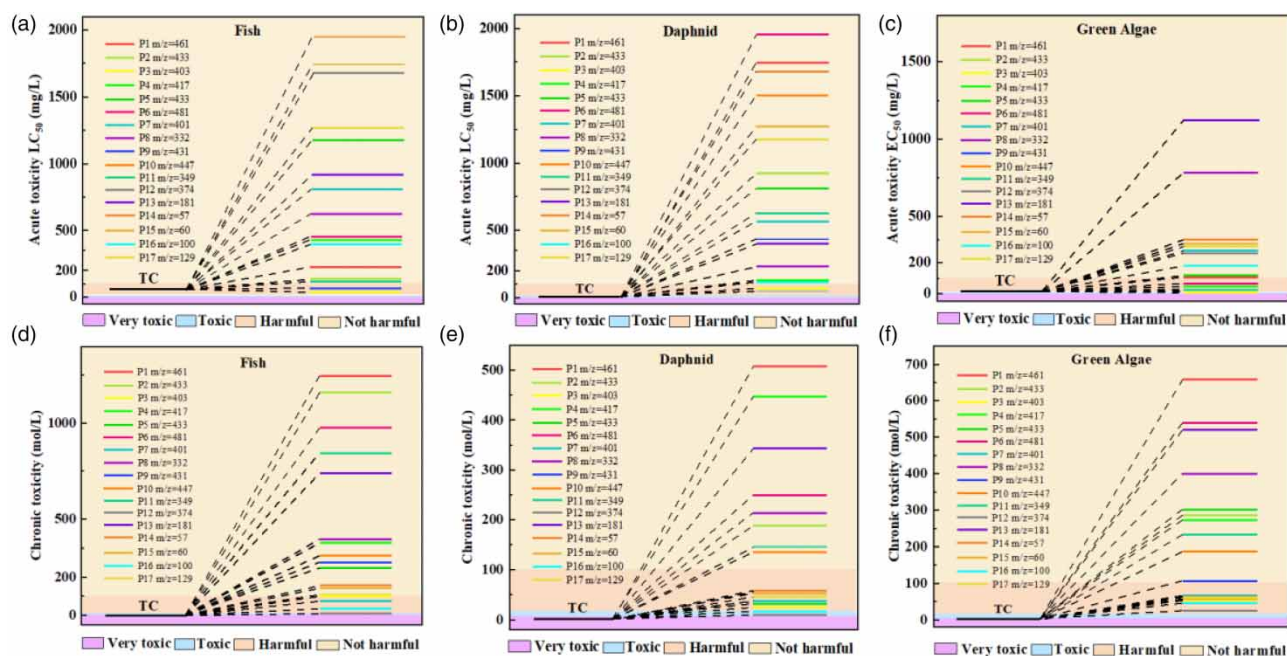


Figure 11 | Acute toxicity of (a) fish LC50 (96 h); (b) daphnid LC50 (48 h); (c) green algae EC50 (48 h); chronic toxicity of (d) fish; (e) daphnid; (f) green algae.

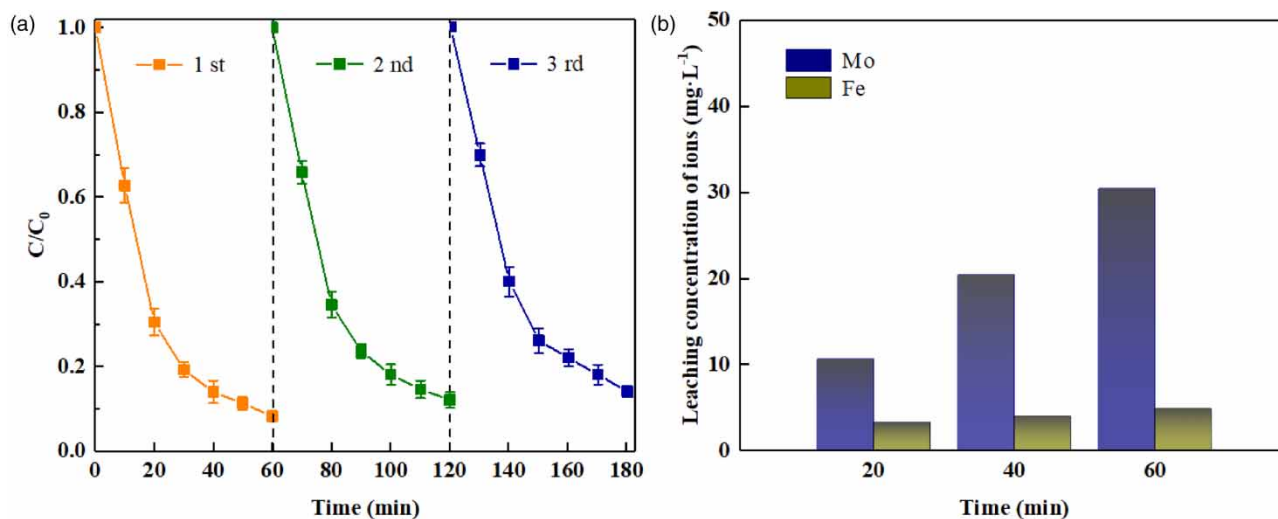


Figure 12 | (a) Recyclability experiments of $\text{MoS}_2/\text{Fe}_3\text{O}_4$ and (b) leaching concentration of metal ions.

surface during the reaction resulted in the decrease in the conversion efficiency of Fe^{3+} to Fe^{2+} . In order to investigate the stability of $\text{MoS}_2/\text{Fe}_3\text{O}_4$, the concentration of Mo and Fe ions leached from $\text{MoS}_2/\text{Fe}_3\text{O}_4$ was monitored by ICP. As shown in Figure 12(b), the concentration of Mo and Fe in the $\text{MoS}_2/\text{Fe}_3\text{O}_4/\text{PS}$ system was only 30.4 and 4.85 $\text{mg}\cdot\text{L}^{-1}$ after 60 min reaction, respectively, which demonstrated its high stability.

4. CONCLUSIONS

In this work, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ was successfully prepared as PS activator to improve the removal of TC and the separation of MoS_2 . Compared to single Fe_3O_4 and MoS_2 , $\text{MoS}_2/\text{Fe}_3\text{O}_4$ had higher activation activity for PS activation, achieving a removal efficiency of 91.8% for 20 $\text{mg}\cdot\text{L}^{-1}$ TC after 60 min under the conditions of 0.4 $\text{g}\cdot\text{L}^{-1}$ $\text{MoS}_2/\text{Fe}_3\text{O}_4$, 4 mmol PS and pH 7. $\text{MoS}_2/\text{Fe}_3\text{O}_4$ also demonstrated favorable stability during recycling experiments. The degradation process of TC in the $\text{MoS}_2/\text{Fe}_3\text{O}_4$ system could be divided into free radical decomposition pathway ($\text{SO}_4^{\bullet-}$, $\bullet\text{OH}$ and $\bullet\text{O}_2^-$) and non-free radical decomposition pathway ($^1\text{O}_2$), with $\bullet\text{OH}$, $\bullet\text{O}_2^-$ and $^1\text{O}_2$ identified as the predominant active species. The three major degradation pathways of TC in the $\text{MoS}_2/\text{Fe}_3\text{O}_4$ system were proposed as hydroxylation, ketylation of dimethylamino group and C-N bond breaking. The toxicity of TC and its intermediates could be effectively reduced by using $\text{MoS}_2/\text{Fe}_3\text{O}_4$ to activate PS. In conclusion, $\text{MoS}_2/\text{Fe}_3\text{O}_4$ prepared was an efficient PS activator to promote the decomposition of refractory organic pollutants.

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AUTHOR CONTRIBUTIONS

L. Z. arranged the resources, wrote the review and edited the article, and rendered support in funding acquisition. Q. Z. investigated the work, rendered support in data curation, and wrote the original draft. T. C. investigated the work and rendered support in data curation. C. W. investigated the work and rendered support in data curation. C. X. investigated the work and edited the article. J. G. supervised the work, arranged the resources, and wrote the review. X. P. investigated the work and edited the article. S. L. validated the article and visualized the data.

DATA AVAILABILITY STATEMENT

All relevant data are included in the paper or its Supplementary Information.

CONFLICT OF INTEREST

The authors declare there is no conflict.

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